A Simplified Physico-Mathematical Model toward Tumor Ablation Therapy by Microbubble Enhanced HIFU

気泡増強集束超音波による腫瘍焼灼治療のための 簡易予測モデルの提案

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1. Introduction

Cancer treatment by High-Intensity Focused Ultrasound (HIFU) [1] is a low invasive method utilizing a thermal coagulation of tumor tissues. A Khokhlov-Zabolotskaya-Kuznetsov (KZK) equation [2] describing weakly nonlinear (i.e., finite but small amplitude) propagation of focused ultrasound in a single-phase liquid has been used as a physicomathematical model for HIFU treatment.

Recently, it is reported that the utilization of microbubbles as an enhancer drastically improves the heating effects of HIFU [3]. Kanagawa et al. [2] has extended the KZK equation for single-phase liquid into that for bubbly liquid. In our previous work [4], thermal conduction at gas-liquid interface is introduced by utilizing the energy equation [5] for gas inside bubble and we then found that the thermal conduction strongly contributes the dissipation effect. However, the phase difference between the temperature gradient at gas-liquid interface and the average temperature of gas inside bubble [6] is neglected. Since temperature of the tumor may rise over 80 degrees in HIFU treatment [1], detailed description of these thermal effects is strongly desired for such an application.

In this study, a KZK equation is re-derived by incorporating the phase difference between the temperature gradient at gas-liquid interface and the average temperature [6].

2. Problem statement

Long-range propagation of ultrasound radiated from circular sound source placed in an initially quiescent liquid non-uniformly containing many spherical microbubbles is theoretically investigated (**Fig. 1**). The main assumptions are summarized as follows: (i) Incident frequency of ultrasound is quite lower than eigenfrequency of bubble oscillations; (ii) Wavelength is quite longer than the bubble radius; (iii) Diameter of circular



Fig. 1 Schematic of the model.

sound source is sufficiently longer than the wavelength, and this leads to the assumption that wavefront is quasi-planar [2, 4]; (iv) Gas inside bubbles is only composed of non-condensable gas, hence the phase change across gas-liquid interface does not occur.

3. Basic equations

The energy equation for single-bubble describing thermal conduction at the bubble-liquid interface is used [5]:

$$\frac{\mathrm{D}_{\mathrm{G}} p_{\mathrm{G}}^*}{\mathrm{D} t^*} = \frac{3}{R^*} \left[(\kappa - 1) \lambda^* \frac{\partial T_{\mathrm{G}}^*}{\partial r_{\mathrm{G}}^*} \right|_{r_{\mathrm{G}}^* = R^*} - \kappa p_{\mathrm{G}}^* \frac{\mathrm{D}_{\mathrm{G}} R^*}{\mathrm{D} t^*} \right], \quad (1)$$

where t^* is the time, p^* pressure, R^* bubble radius, κ ratio of specific heats of gas, λ^* thermal conductivity of gas, T^* temperature; the subscript G denotes volume-averaged variables in gas phases, subscript 0 does the quantities in the initial uniform state at rest, and superscript * does a dimensional quantity. Temperature gradient $\partial T^*_G / \partial r^*_G |_{r^*_G = R^*}$ in Eq. (1) is rewritten by the following model considering the phase difference between the temperature gradient at gas-liquid interface and the average temperature of gas inside bubble [6]:

$$\frac{\partial T_{\rm G}^*}{\partial r_{\rm G}^*}\Big|_{r_{\rm G}^*=R^*} = \frac{{\rm Re}(\tilde{L}_{\rm P}^*)}{\left|\tilde{L}_{\rm P}^*\right|^2}(T_0^*-T_{\rm G}^*) + \frac{{\rm Im}(\tilde{L}_{\rm P}^*)}{\omega_{\rm B}^*\left|\tilde{L}_{\rm P}^*\right|^2}\frac{{\rm D}_{\rm G}T_{\rm G}^*}{{\rm D}t^*}, \quad (2)$$

where $\tilde{L}_{\rm P}^*$ is the complex number having the dimension of length [6] and $\omega_{\rm B}^*$ eigenfrequency of bubble oscillation. Furthermore, the conservation laws of mas and momentum for bubbly liquids based

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of two fluid-model [7], the momentum conservation for a spherical symmetric oscillating bubble in a compressible liquid, Tait equation of state for liquid, equation of state for ideal gas inside bubble, conservation equation of mass inside bubble, and balance of normal stresses at the bubble-liquid interface are also introduced (see the explicit forms in Refs. [2, 4]).

4. Results

All the dependent variables are expanded in power series, e.g., the expansion of T_{G}^{*} is

$$\frac{T_{\rm G}^*}{T_{\rm G0}^*} = 1 + \epsilon T_{\rm G1} + \epsilon^2 T_{\rm G2} + \cdots,$$
(3)

where ϵ ($\ll 1$) is a typical nondimensional (finite but small) amplitude of the ultrasound. As in the same manners of Refs. [2, 4], we can derive the KZK equation in terms of temperature T_{G1} :

$$\frac{\partial}{\partial \tau} \left(\frac{\partial T_{G1}}{\partial \xi} + \Pi_1 T_{G1} \frac{\partial T_{G1}}{\partial \tau} + \Pi_{21} \frac{\partial^2 T_{G1}}{\partial \tau^2} + \Pi_{22} T_{G1} + \Pi_3 \frac{\partial^3 T_{G1}}{\partial \tau^3} \right) = \frac{\Gamma^2}{2\zeta} \frac{\partial}{\partial \zeta} \left(\zeta \frac{\partial T_{G1}}{\partial \zeta} \right),$$
(4)

via a variables transform as retarded time expression,

$$\tau = t - (1 + \Pi_0)x, \ \xi = \epsilon x, \ \zeta = \sqrt{\epsilon}\Gamma r, \tag{5}$$

where Γ is the quantity of O(1) representing the size of focusing of ultrasound. The right-hand side of Eq. (4) represents the focusing along the radial direction. The term with coefficient Π_0 , Π_1 and Π_3 represent the advection, nonlinearity and dispersion effects, respectively, both Π_{21} and Π_{22} the dissipation effects. Advection coefficient Π_0 and dissipation coefficient Π_{22} are

$$\Pi_{0} = \frac{(1-\alpha_{0})U^{*2}}{6\alpha_{0}c_{L0}^{*2}} \left[\frac{\omega_{B}^{2*}R_{0}^{*2}}{\omega^{*2}L^{*2}} - \frac{3(\gamma_{e}-\kappa)p_{G0}^{*}}{\rho_{L0}^{*}U^{*2}} \right] \\
- \frac{2L^{*2}}{3\alpha_{0}R_{0}^{*2}} \left(\frac{\mu_{e0}^{*}}{\rho_{L0}^{*}U^{*}L^{*}} \right)^{2} \qquad (6) \\
- \frac{3(\kappa-1)^{2}[\alpha_{0}(1-\alpha_{0})+\beta_{1}]\lambda^{*}}{2\beta_{1}\alpha_{0}(1-\alpha_{0})\rho_{L0}^{*}U^{*2}R_{0}^{*}\epsilon} \frac{\mathrm{Im}(\tilde{L}_{P}^{*})T_{0}^{*}}{\omega_{B}^{*}|\tilde{L}_{P}^{*}|^{2}} \\
\Pi_{22} = \frac{3(\kappa-1)^{2}[\alpha_{0}(1-\alpha_{0})+\beta_{1}]\lambda^{*}}{2\beta_{1}\alpha_{0}(1-\alpha_{0})\rho_{L0}^{*}U^{*2}\omega^{*}R_{0}^{*}\epsilon} \frac{\mathrm{Re}(\tilde{L}_{P}^{*})T_{0}^{*}}{|\tilde{L}_{P}^{*}|^{2}}, \qquad (7)$$

where L^* , U^* , ω^* are typical wavelength, wave speed, incident frequency of the ultrasound, α void fraction, c_{L0}^* wave speed in pure water, γ_e and μ_e^* are effective polytropic exponent and viscosity [6]. The last term of advection coefficient Π_0 (Eq. (6)) arises from the imaginary part of Eq. (2), hence the phase difference between the temperature gradient and the average temperature affects the advection



Fig. 2 Dissipation coefficient Π_{22} versus the initial void fraction α_0 for the normal condition of air-water system in our previous study [4] and present study.

effect.

Dissipation coefficient Π_{22} arises from the thermal conduction at gas-liquid interface (the real part of Eq. (2)). Fig. 2 shows the dependence of Π_{22} on α_0 in our previous study [4] and present study, and then we found that thermal conduction more strongly affects the dissipation effect in this study.

5. Summary

We have derived a KZK equation for a nonlinear propagation of focused ultrasound in bubbly liquids incorporating the thermal conduction at the gas-liquid interface by Eq. (1). Temperature gradient term in Eq. (1) is rewritten by Eq. (2) considering the phase difference between the temperature gradient at gas-liquid interface and the average temperature of gas inside bubble. As a result, the phase difference affects the advection effect and the thermal conduction more strongly affects the dissipation effect than in our previous work [3].

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